



AN EXPERIMENTAL STUDY OF PRESSURE LOSSES IN A WET VACUUM DRUM DEVICE

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Abstract

The article presents the results of an experimental study in an experimental setup, a drum wet dust cleaning apparatus under various gas and liquid flow regimes. The local and general coefficients of resistance and the loss of total pressures in the working sections of the device are determined. As a result, depending on these pressures, it is possible to determine the optimal values of the efficiency of dust and gas cleaning and the energy consumption of the device.

Keywords: wet method, drum, screen, gas flow, liquid flow, pressure, dust, speed, apparatus.

Introduction

Today, as a result of the development of industry on a global scale, the level of atmospheric air pollution is increasing. The amount of emissions released into the atmosphere from chemical, building materials, and hydrometallurgical industries is especially high [1,7,8,9]. To solve these problems, dust and gas cleaning devices with different structural structures are being created and scientific research is being carried out worldwide [2,3,4,5,6]. The main requirements for the devices being created are the simplicity of the construction structure, high cleaning efficiency and low energy consumption. Based on these requirements, we have developed a new structure of the apparatus working in the wet method and are conducting scientific research [10].

Materials and Methods

The kinematic diagram of the newly created drum dust cleaning device is shown in Fig. 1 and the general view is shown in Fig. 2.

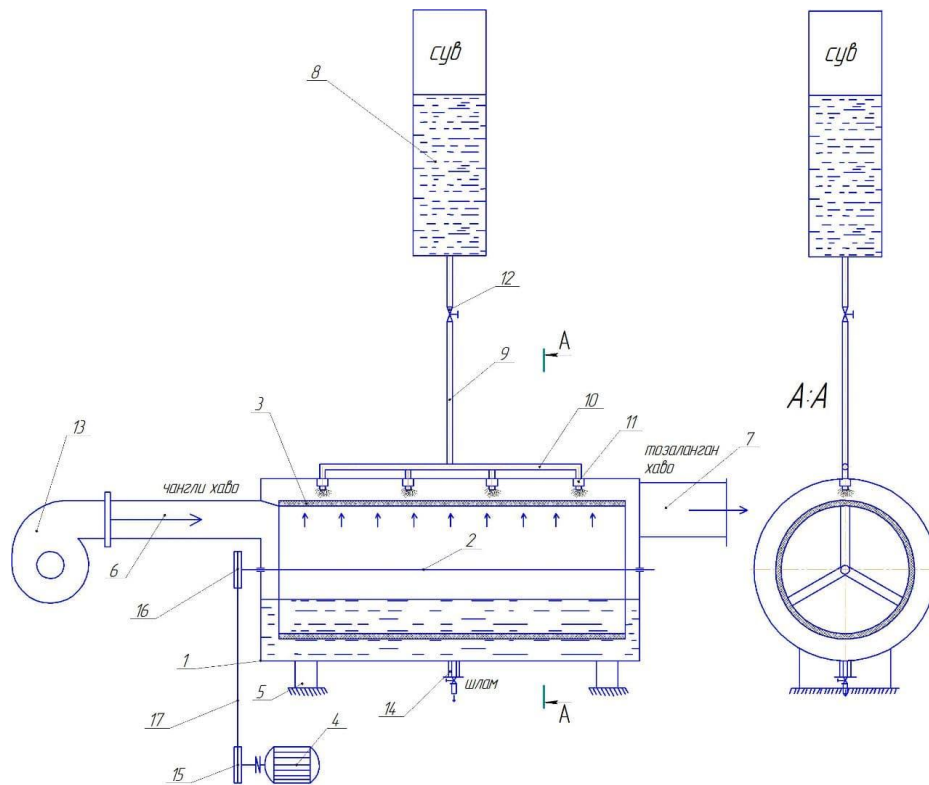


Figure 1. Scheme of the device with a wet dust cleaning drum

1. Cylinder body, 2. Shaft, 3. Drum, 4. Electric motor, 5. Support, 6. Dust air inlet pipe, 7. Purified air outlet pipe, 8. Water tank, 9. Water transfer pipe, 10. Water distribution pipe, 11-stuck, 12-water valve. 13-fan, 14-sludge valve, 15-drive pulley, 16-drive, 17-belt.



Figure 2. Overview of the drum device.

Theoretical studies were carried out to calculate the drum device. As a result, the equation for calculating the total pressure in the apparatus was derived [10,11].

$$P_{o\delta} = \lambda_1 \cdot \frac{l}{d} \cdot \rho_{cm} \cdot \frac{\omega_{cm}^2}{2} + \Delta\Pi \frac{\sum S_c \cdot \delta}{\sum S_c \cdot a} \cdot \frac{\rho_{cm} \cdot \omega_{cm}^2}{2} + \lambda_2 \cdot \frac{l}{d} \cdot \rho \cdot \frac{\omega^2}{2} \quad (1)$$

where λ_1 is the coefficient of friction with the pipe wall that transmits dust gas to the device, l is the length of the pipe through which dust gas moves, m ; d -pipe diameter, m ; ρ_{sm} -dusty air mixture density, kg/m^3 ; velocity of dusty air mixture moving in ω_{sm} -pipe, m/s . The density of the mixture.

ω_{sm} is the movement speed of the dusty air mixture on the surface of the drum screen, m/s ; ξ_c is the resistance coefficient of the drum grid.

The theoretical total resistance coefficient of the device is equal to (2,3) [10].

$$\xi_{ym} = \xi_k + \xi_c + \xi_u \quad (2)$$

$$\xi_{ym} = \lambda_1 \frac{l}{d} + \Delta\Pi \frac{\sum S \cdot \delta}{\sum S \cdot a} + \lambda_2 \frac{l}{d} \quad (3)$$

The overall resistance coefficient of the drum sieve is determined as follows depending on the surface of the dusty air passing through the sieve [10-17].

$$\xi_c = \Delta\Pi \frac{\sum S_c \cdot \delta}{\sum S_c \cdot a}, \quad (4)$$

where ΔP is the correction coefficient, determined by experiments, $\sum S_c$ - the total surface of the part through which dusty air passes through the grid, m^2 ; δ -thickness of mesh wire, m ; dimensions of the square hole of a mesh, m ; where λ_2 is the coefficient of friction in the exhaust pipe of purified air; l - length of the pipe through which purified air moves, m ; d -pipe diameter, m ; ρ -purified air density, kg/m^3 ; velocity of purified air moving in the ω -pipe, m/s .

Results

The fan in the experimental determination of the coefficient of resistance of the device the gas consumption in the suction part, the fan installed in the device body, and the gas consumption coming out of the device were determined. The local resistance coefficients of the apparatus were determined from the difference in gas consumption. The local resistance of the device was $\xi_M=0,35$. To simplify calculations, formula 3 looks like this.

$$\xi_y = 0,35 + \Delta P \frac{\sum S_c \cdot \delta}{\sum S_c \cdot a} \quad (5)$$

At the next stage of the experiments, a square hole size $a=0.6, 0.8, 1$ mm was wrapped around the working drum to form a drum. According to the results, the resistance coefficient $\xi_c=2$ when the mesh square hole size is $a=0.6$ mm, the mesh wire thickness is $\delta=0,25$, the hole size is $a=0.8$ mm, and the mesh wire thickness is $\delta =0.325$ mm $\xi_c =1,8$; $\xi_c=1.6$ when the hole size is $a=1$ mm, and the thickness of the grid wire is $\delta =0.4$ mm. Based on the obtained results, a graph is constructed (Fig. 2).

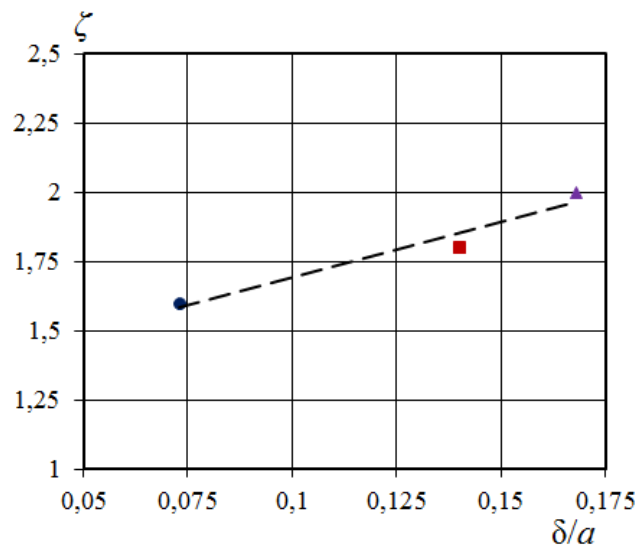


Figure 2. The graph of the change of the resistance coefficient depending on the size of the mesh installed on the device

The resulting regression equation looks like this.

$$y = 3.9866x + 1.2937 \quad R^2 = 0.9468$$

Based on the results of the experimental study, the correction coefficients for determining the grid resistance coefficients were determined (Table 1).

Table 1. The results of experiments to determine the correction coefficient

No	Setka square hole dimensions; a, mm	The thickness of the wire; δ , mm	The number of wires in the set; n, piece	Resistance coefficient; ξ	Correction factor ΔP
1	0.6	0.25	1176	1.65	17.6
2	0.8	0.325	888	1.45	17
3	1.0	0.4	714	1.25	16

In the next stage of the experiments, the pressure loss was determined when the mesh was installed in the apparatus body without spraying water and when water was sprayed. The obtained experimental results were processed based on a computer program and a graph was constructed (Fig. 3).

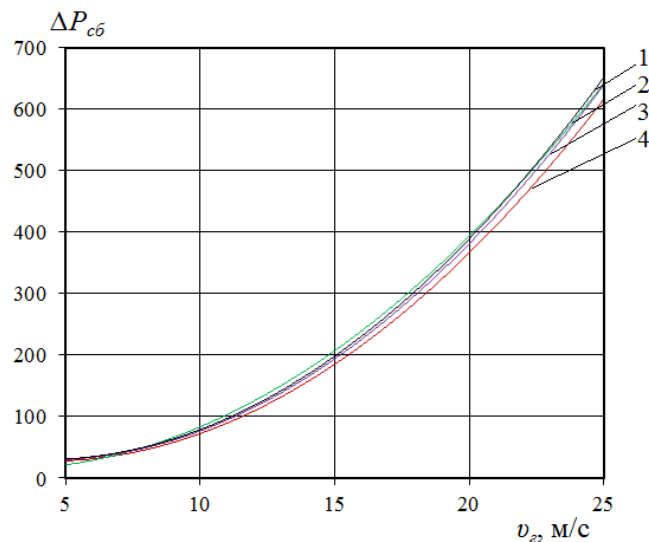


Figure 3. The graph of the change of the lost pressure depends on the gas velocity.

(unwatered)

1-d=0.6mm; 2-d=0.8mm; 3-d=1mm;

The resulting regression equations are as follows

$$y = 1.407x^2 - 11.76x + 53.5 \quad R^2 = 0.9843$$

$$y = 1.4264x^2 - 11.787x + 54.088 \quad R^2 = 0.9849$$

$$y = 1.2384x^2 - 6.1803x + 21.296 \quad R^2 = 0.9979$$

$$y = 1.3665x^2 - 11.608x + 51.668 \quad R^2 = 0.9846$$

Fixed gas consumption $Q=141 \div 732 \text{ m}^3/\text{hour}$ (with the step of $141 \text{ m}^3/\text{hour}$) was given to the meeting drums with square hole sizes $a=0.6, 0.8,$ and 1 mm separately. In each gas consumption, the device connected to the drummer was sprinkled from 4 S32-412 brand nozzles $Q_s=0.075 \div 0.3 \text{ m}^3/\text{hour}$ (with a step of $0.075 \text{ m}^3/\text{hour}$). At each step of the water sprinkled on the selected grids, gas velocities and flow rates were determined. The total resistance coefficients in the case of the device being sprinkled with water were determined by the differences in gas consumption.

The total pressure lost depending on the determined resistance coefficients and gas velocities for each mode was determined. The obtained experimental results were processed based on the computer program and graphs of dependence were built (Figures 3, 4, 5, 6).

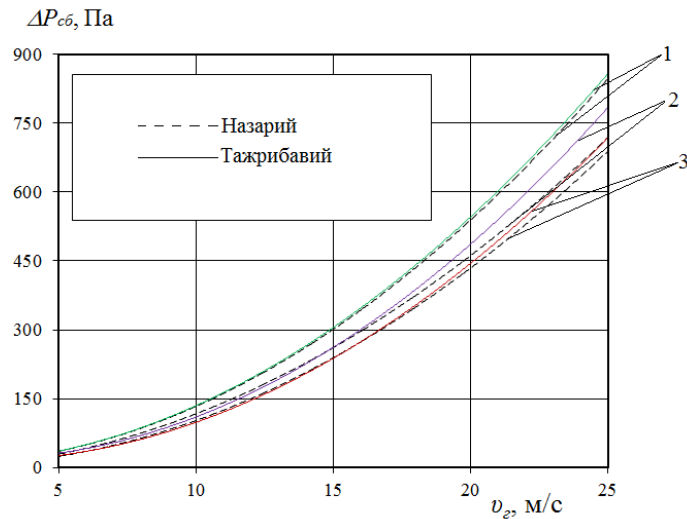


Figure 4. Dependence of the total pressure loss on the gas velocity when the liquid consumption is $Q_s=0.075 \text{ m}^3/\text{h}$ - const.

The resulting regression equation looks like this

$$y = 1.3665x^2 - 11.608x + 51.668 \quad R^2 = 0.9846$$

$$y = 1.4563x^2 - 6.0986x + 25.67 \quad R^2 = 0.9988$$

$$y = 1.3423x^2 - 5.6846x + 21.27 \quad R^2 = 0.9996$$

$$y = 1.4147x^2 - 1.3914x + 7.586 \quad R^2 = 0.9999$$

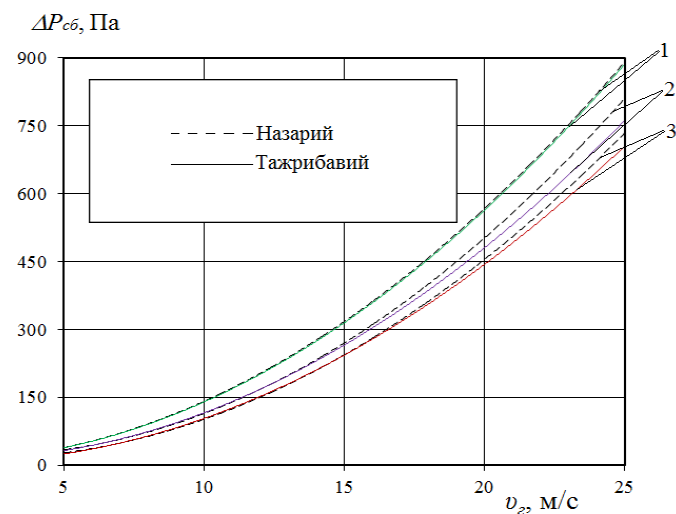


Figure 5. Dependence of the total pressure loss on the gas velocity when the fluid consumption is $Q_s=0.150 \text{ m}^3/\text{h}$ -const.

The resulting regression equation looks like this.

$$y = 1.2384x^2 - 6.1803x + 21.296 \quad R^2 = 0,9979$$

$$y = 1.3681x^2 - 5.7122x + 21.856 \quad R^2 = 0,9996$$

$$y = 1.518x^2 - 6.758x + 30.23 \quad R^2 = 0.9984$$

$$y = 1.4715x^2 - 1.5511x + 9.866 \quad R^2 = 0,9997$$

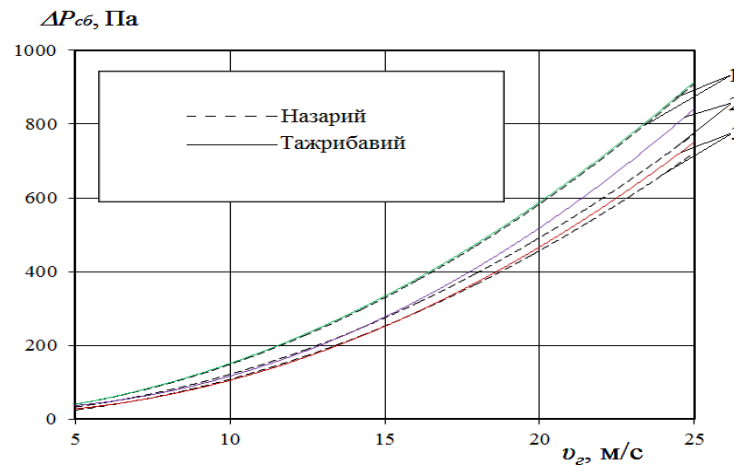


Figure 6. Dependence of the total pressure loss on the gas velocity when the fluid consumption is $Q_s=0.225 \text{ m}^3/\text{h}$ - const.

The resulting regression equation looks like this.

$$y = 1.407x^2 - 11.76x + 53.5 \quad R^2 = 0.9843$$

$$y = 1.3785x^2 - 5.2229x + 19.744 \quad R^2 = 0,9997$$

$$y = 1.6174x^2 - 8.3427x + 38.432 \quad R^2 = 0.998$$

$$y = 1.4376x^2 + 0.5688x + 1.684 \quad R^2 = 0,9994$$

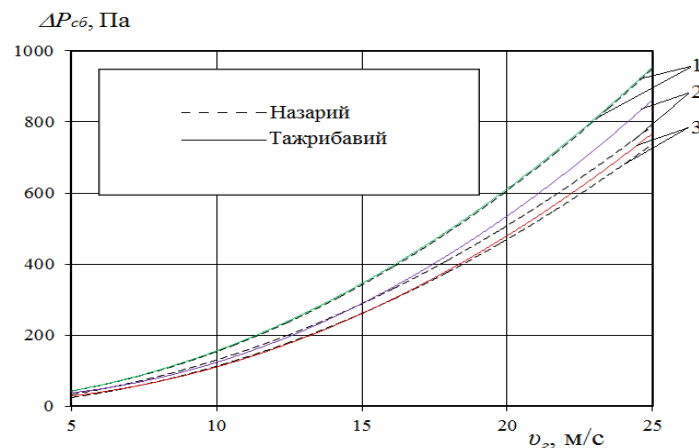


Figure 7. Dependence of the total pressure loss on the gas velocity when the liquid consumption is $Q_s=0.3 \text{ m}^3/\text{h}$ -const.



The resulting regression equation looks like this.

$$y = 1.4264x^2 - 11.787x + 54.088 \quad R^2 = 0,9849$$

$$y = 1.3721x^2 - 4.2562x + 15.886 \quad R^2 = 0,9997$$

$$y = 1.6017x^2 - 6.9114x + 32.53 \quad R^2 = 0.9979$$

$$y = 1.5273x^2 - 0.3005x + 6.406 \quad R^2 = 0$$

When the diameter of the 1st mesh is $d=0.6$ mm; When the diameter of the 2nd mesh is $d=0.8$ mm; When the diameter of the 3rd mesh is $d=0.6$ mm;

It can be seen from the graphs presented in the above figures 4, 5, 6, and 7 that the value of the lost pressure increases with the decrease in the size of the mesh holes at constant fluid consumption. The value of the lost total pressure also increased when the liquid consumption was changed in the interval $Q_s=0.150\div 0.3$ m³/h (with a step of 0.075 m³/h). The error between the theoretical and experimental values of the lost total pressure does not exceed $\Delta=5\%$. The conducted experimental studies fully confirmed the proposed formula 1.

Conclusion

In the article, the results of the experimental study of the wet dust cleaning drum apparatus in the pilot plant, in different gas and liquid flow regimes, were presented. Local and general resistance coefficients and lost total pressures in the working parts of the device were determined. As a result, depending on these pressures, it was possible to determine the optimal values of the dust gas cleaning efficiency and energy consumption of the device.

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